

### **MEMORANDUM**

TO:

Jim Eddinger, U.S. Environmental Protection Agency (C439-01)

FROM:

Chad Leatherwood, Eastern Research Group

DATE:

October, 2002

SUBJECT:

Development of Fuel Switching Costs and Emission Reductions for

Industrial/Commercial/Institutional Boilers and Process Heaters National

EPA AIR DOCKET

Emission Standards for Hazardous Air Pollutants

### 1.0 INTRODUCTION

The purpose of this memorandum is to discuss the cost and emission impacts resulting from fuel switching in boilers and process heaters. Fuel switching is a potential control option that would require some boilers and process heaters to convert to natural gas, which emits lower emissions of some compounds when combusted than most solid and liquid fuels such as coal and residual oil. For many pollutants, fuel switching generally results in greater emission reductions than add-on technologies, and for some pollutants, fuel switching may be the only control method available.

For this analysis, the cost, emission, and operational impacts of fuel switching coal-fired and residual oil-fired boilers and process heaters to natural gas were examined. It was assumed that units burning biomass, non-fossil fuel, or wood, alone or in combination with gaseous fuel, would be unlikely to fuel switch to natural gas alone. This assumption is based on the availability of the current fuel blend, the cost differential between the current fuel blend and natural gas, and the limited emission reductions that would be achieved over add-on control devices. Similarly, it was assumed that units burning distillate oil would not fuel switch because of the limited emission reduction that would be achieved.

Section 2.0 summarizes the results of the analysis. Section 3.0 discusses the analysis in more detail, and Section 4.0 presents references. Detailed calculation tables are in Attachment A.

### 2.0 RESULTS OF ANALYSIS

Table 2-1 summarizes the capital investment and annual costs estimated for fuel switching coal-fired and residual oil-fired boilers and process heaters to natural gas. Fuel switching would require over \$3 billion in capital costs and \$12 billion in annual costs. Of these totals, units firing coal, either wholly or partially, incur 66 percent of the capital and 83 percent of the annual costs. Additionally, 93 percent of the capital and 94 percent of the annual costs are from fuel switching boilers.

Table 2-1. Summary of Capital and Annual Costs for Fuel Switching to Natural Gas

100000000000000000000000000000000000000	Fuel	Capital Costs (\$ 1,000,000)	Annual Costs (\$1,000,000/yr)
	Coal	2.092	10,644
	Residual Oil	868	1.383
Boilers	Total	2.960	12,026
	Coal	0	0
	Residual Oil	215	826
Process Heaters	Total	215	826
	Coal	2,092	10,644
	Residual Oil	1,083	2,208
Total	Total	3,175	12,851

Table 2-2 summarizes the emission reductions for selected pollutants as a result of fuel switching. Emissions of metallic, inorganic, and some organic compounds decrease as a result of fuel switching. However, emissions of some organic compounds, such as formaldehyde, would increase with fuel switching.

Table 2-2. Summary of Emission Reductions of Selected Compounds from Fuel Switching (Mg/yr)

				Metals			Acid Gases	ases		Organics	ıcs	
Combustor	Fuel	Arscuic	Chromium	Lead	Manganese	Mercury	Hydrogen Chloride	Hydrogen Fluoride	Acetaldehyde	Benzene	Formalde hyde	Poluene
Boilers	Coal	70	77	100	432	6.1	53,216	4,583	-64	505	211	91
	Residual Oil	2		5.8	510	3.4	22	0	-100	3.0	-79	4.
	Total	72	88	901	943	9.5	53,238	4,583	-164	508	132	30
Process Heaters	Coal	0	0	0	0	0	0	0	0	0	0	0
	Residual Oil	0.5	2.7	1.4	126	0.8	5.3	0	-23	0.7	61-	3.3
	Total	0.5	2.7	4.1	126	8.0	5.3	0	-23	0.7	-19	3.3
Total	Coal	70	77	001	432	6.1	53,216	4,583	-64	505	211	91
	Residual Oil	2.5	14	7.2	636	4.2	27	0	-123	3.7	86-	17
	Total	73	91	107	1.069	01	53.243	4.583	-187	509	113	33

### 3.0 DESCRIPTION OF ANALYSIS

### 3.1 Background

A portion of the work products developed by the Industrial Combustion Coordinated Rulemaking (ICCR) Federal Advisory Committee Act were databases that contained an inventory of the population of boilers, process heaters, IC engines, turbines, and incinerators in the nation. Detailed information about these databases can be found in other memoranda.<sup>1-5</sup>

A review of the population databases indicated that each boiler or process heater (that does not solely burn natural gas) could be categorized into three scenarios involving fuel switching to natural gas.

- A. The boiler or process heater already uses natural gas as a start-up or back-up fuel. Therefore, it would only require modifications to the boiler or process heater to burn natural gas only.
- B. The boiler or process heater does not use natural gas as a start-up or back-up fuel, but the facility does use gas for some operation on site. This would require modifications to the boiler or process heater and upgrades to the on-site gas handling system.
- C. The facility does not use natural gas at all. This would require modifications to the boiler or process heater, construction of an on-site gas handling system, and construction of piping from the most accessible main gas line.

Additionally. Scenario C was further divided into four cases to address the potential availability of natural gas for boilers and process heaters.

- C1: The main gas line is close to the plant, but the plant is in a city or near a city. Therefore, a higher cost per foot of pipe would be incurred.
- C2: The main gas line is a moderate distance from the plant, and the plant is in a rural location. A lower cost per foot of pipe would be incurred.
- C3: The main gas line is far from the plant, and the plant is in a rural location. A lower cost per foot of pipe would be incurred.
- C4: Gas is not available at all.

Each boiler and process heater in the population database was assigned to one of the above scenarios/cases.

### 3.2 Assignment of Boilers and Process Heaters to Fuel Switching Scenarios

The ICCR population database for boiler and process heaters identify whether a unit already co-fires natural gas. Those that do were assigned to Scenario A. Any boiler or process heater not identified as firing natural gas, but located at a facility that does have another combustion unit firing natural gas was assigned to Scenario B. It was assumed that a natural gas line was available at the facility, so costs incurred for fuel switching the boiler or process heater would be for modification of the on-site gas handling system and for boiler or process heater combustor modifications.

Model units were used to represent the national population of boilers and process heaters. Boilers and process heaters were assigned to models based on the fuel burned, capacity, and combustor type. A detailed discussion of model units is presented in another memorandum. Capacity data were not available for all boilers and process heaters, so units with unknown capacities were assigned to models based on fuel and combustor type using the same distribution (i.e., relative percentages of population) as that for units with known capacities. Attachments A-1 and A-2 present the distribution of boilers and process heaters to Scenarios A and B.

Scenario C units were assumed to be all the boilers and process heaters that were not assigned to scenarios A or B. The boiler and process heaters databases do not provide any information that could be used to assign units to the Scenario C cases. It was assumed that the majority of Case C units would be in case C2 because the widespread use of natural gas lines.<sup>7</sup> To provide a conservative estimate of costs, the majority of the remaining units were assumed to be in case C3, then C1. It was also assumed than only a very small number of boilers and process heaters would not have gas available at all, case C4. For this analysis, case C units were distributed in the following percentages: C1=5%, C2=84%, C3 = 10%, and C4=1%.

### 3.3 Development of Cost Inputs and Factors

Costs were estimated using 1997 as the base year. Information used to calculate capital and annual costs for fuel switching were obtained from two sources: (1) a feasibility study from 1986 on converting oil- and coal-fired utility boilers to fire gas intermittently<sup>8</sup>, and (2) a Phase II

NOx control report. The equations used to calculate capital and annual costs are provided in Attachment A-3. Costing inputs are summarized in Attachment A-4.

Capital Costs. The 1986 feasibility study provided detailed capital cost breakdowns, in dollars per kilowatt of capacity (\$/kW), for fuel switching to natural gas for five utility boilers at five different sites. For this analysis, it was assumed that capital costs for intermittent use of natural gas at utility boilers could be used for continuous use of natural gas by industrial/institutional/commercial boilers and process heaters. Attachment A-5 presents the cost components from the 1986 document. The attachment lists the costs of each component from the five studies found in the 1986 feasibility study. For the five utility boilers studied, different breakdowns, component groupings, and component names were used. Similar components were grouped together based on descriptions provided and engineering judgment. The table also allocates components to either the gas handling system, combustor system, or "other" (administrative, vendor representative, startup, etc).

Attachment A-6 presents the costs calculated for each scenario. Components were assigned to scenarios A and B using engineering judgment based on the costs that would probably be incurred for each scenario. The average costs for gas systems or combustor systems were calculated for each case and added to the "other" costs to obtain the total cost of fuel switching for each case. Average costs were used to account for differences between the studies and to provide a normalized cost factor. It was assumed that each case would require "other" costs. Costs were escalated from 1985 dollars to 1997 dollars using the Chemical Engineering plant cost indices.<sup>10</sup>

For the scenario C cases C1, C2, and C3, the only additional costs beyond those for Case B are the costs for the piping and piping installation (e.g., Case C1 cost = Scenario B cost + Case C1 piping cost). For this analysis, the pipe lengths used in cost estimates were 500 feet for case C1. I mile for case C2, and 10 miles for case C3. Pipe lengths were based on engineering judgment, information provided in the feasibility study, and a study of pipelines in the United States. The cost per foot of pipe was determined based on whether the scenario would be in a city or a rural area. Using information in the feasibility study, a cost of \$125 per foot of pipe was used for pipelines in a city (case C1) and a cost of \$25 per foot of pipe was used for pipelines in a rural location (cases C1 and C2). The higher cost for city pipelines are due to greater

construction costs to install pipelines in smaller, more congested areas. For case C4, because gas is not available, the cost of add-on controls was used. The cost of add-on controls is discussed in another memorandum.<sup>11</sup>

<u>Total Annual Costs</u>. The components of total annual costs for fuel switching that apply to industrial boilers and process heaters include:

- Annualized capital
- Difference in fuel costs between natural gas and current fuel blend
- Efficiency loss due to fuel switching
- SO<sub>2</sub> Allowances
- Capacity recovery

SO<sub>2</sub> allowances and capacity recovery were not included in the analysis because there was insufficient information to estimate them. Additionally, they are not considered to be as significant as the annualized capital costs and annual fuel cost differences, and their exclusion should not have a significant impact on the results of the analysis. Annualized capital costs were estimated using an interest rate of 7 percent and assuming that the fuel switching equipment has a 20-year life span (equal to a capital recovery factor (CRF) of 0.09439). The 7 percent interest rate is the current rate used in EPA analyses.

Differences in fuel costs were calculated based on the prices obtained from the Department of Energy (DOE) Energy Information Administration (EIA) database for 1997<sup>12</sup>, and converted to a dollars per million Btu (\$/MMBtu) basis:

Coal cost = \$35.72/metric ton = \$1.35/MMBtu

assuming 12,000 Btu per lb heating value<sup>13</sup>

Gas cost = \$3.59/thousand standard cubic feet = \$3.52/MMBtu

assuming 1.020 Btu per scf heating value<sup>13</sup>

Residual Oil cost = \$2.90/MMBtu

For this analysis, it was also assumed that each unit would operate 8,400 hours per year (i.e., two weeks down time per year).

The 1986 feasibility study provides an average efficiency loss of 5 percent when converting to natural gas. This value was used to calculate the additional heat input required to overcome the loss. The equations used to calculate capital and annual costs are provided in Attachment A-3. Costing inputs are summarized in Attachment A-4.

### 3.4 <u>Calculation of Cost Impacts</u>

Capital and annual costs of fuel switching all of the boilers and process heaters assigned to each applicable model unit (i.e. coal or residual oil-fired models) are presented in Attachment A-7. For this analysis, it was assumed that models co-firing any amount of coal would completely fuel switch to natural gas instead of replacing coal with another fuel. This provides a conservative cost estimate of costs from these models. More detailed calculation tables are found in Attachments A-8 and A-9. Attachments A-10 and A-11 present the calculation of Scenario C capital costs assuming inputs for cost of pipe, length of pipe, and percentage of model units that comprise each case. Attachment A-12 compares the costs of fuel switching to the costs of add-on control technologies for each model.

### 3.5 <u>Calculation of Emission Impacts</u>

Attachments A-13 and A-14 present the emission reductions for selected compounds from fuel switching for each boiler and process heater model, respectively. Emission reductions from fuel switching were calculated by subtracting emissions estimated from burning natural gas from emissions estimated from burning the existing fuel(s). Emissions from combusting the existing fuel were calculated for the baseline emissions analysis and are discussed in another memorandum. Emissions from using natural gas only were calculated using emission factors developed for the baseline emissions analysis. Emission factors for natural gas combustion are discussed in detail in another memorandum. As stated in Section 2.0, emissions for most pollutants are reduced by fuel switching. However, for some organic compounds that are present in larger quantities in natural gas than coal, such as acetaldehyde and formaldehyde, increases in emissions (represented by a negative number) were predicted. Attachment A-15 compares the fuel switching emission reductions to reductions achieved using add-on control technologies.

### 4.0 REFERENCES

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- 4. David Rhodes, ERG. Memorandum to Fred Porter and Jim Eddinger, U.S. Environmental Protection Agency. *Description of Fields in the ICCR Survey Database Version 3.0.* September 8, 1999.
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- 8. <u>Feasibility and Cost of Converting Oil- and Coal-fired Utility Boilers to Intermittent Use of Natural Gas</u>, Fay, James A., et al., Massachusetts Institute of Technology, December 1986.
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- 14. Christy Burlew, ERG. Memorandum to Jim Eddinger, U.S. Environmental Protection Agency, OAQPS. Development of Average Emission Factors and Baseline Emissions Estimates for the Industrial, Commercial, and Institutional Boilers and Process Heaters National Emission Standards for Hazardous Air Pollutants. October, 2002.

### APPENDIX A

### **Detailed Cost and Emission Reduction Tables**

(See Excel spreadsheet "Fswitchappa.xls")

	ing to the second of the secon	Model Parameters (	Model Parameters (Capacity in MMBtu/hr)				Known	Z.	Assı	Assumed * **********************************	*	Total	
20,500				, , , , , , , , , , , , , , , , , , ,	gerlan	Final #			Bollers w/o Capacity Data	Boilers w/o Capacity Data			
Model	Material		Compustor Type	Capacity Range	Avg Capacity	of Units	Case A	Case B	distributed into Model - Case A	distributed into Model - Case B	Case A	Case B	Case C
-	Coal		Other	0-10	4	83	2	5	3	8	5	13	64
2	Coal	•	Other	10-100	\$	919	87	164	105	197	192	361	366
е	Coal	i.,,	Other	100-250	166	509	54	100	09	110	114	210	185
4	Coal	· ·	Other	>250	595	204	52	16	25	16	90	32	122
9	Coat		Wall-fired/PC	0-10	7	12	-	2	-	က	2	5	ည
9	Coal		Wall-fired/PC	10-100	25	86	25	9	33	8	28	14	56
7	Coal		Wall-fired/PC	100-250	186	212	58	35	39	47	89	82	63
80	Coal	<del>- 10 -</del>	Wall-fired/PC	>250	009	291	48	32	99	44	114	9/	100
6	Coal/Wood/NFF Liquid/NFF Solid		All	0-10	9	7	Э		0	0	0	,	9
2	Coal/Wood/NFF Liquid/NFF Solid		NA NA	10-100	35	29	8	4	0	0	∞	4	55
=	Coal/Wood/NFF Liquid/NFF Solid		All	100-250	173	18	4	6	0	-	4	10	4
12	Coal/Wood/NFF Liquid/NFF Solid		All	>250	565	77	31	19	-	-	32	20	26
40	Residual Liquid FF		All	0-10	ო	477	91	27	32	55	48	82	347
4	Residual Liquid FF		All	10-100	37	1,154	90	81	79	129	129	210	815
42	Residual Liquid FF		All	100-250	172	264	31	37	40	48	71	85	108
43	Residual Liquid FF	- 1,	- All	>250	547	141	61	17	25	22	44	33	58
47	Coal	<del>:</del>	Other	0-10	4	36	0	0	0	0	0	0	36
48	Coal		Other	10-100	54	20	2	19	က	59	φ	48	18
49	Coal		Other	100-250	466	59	-	2	7	=	က	16	0
25	Coal	<u></u>	Other	>250	565	7	2	0	2	0	4	0	4
52	Coal	- <del></del>	Wall-fired/PC	10-100	25	32	_	2	4	18	ß	23	S.
53	Coal		Wall-fired/PC	100-250	186	6	0	0	0	0	0	0	6
25	Coal		Wall-fired/PC	>250	009	15	4	0	89	0	15	0	က
55	Coal/Wood/NFF Liquid/NFF Solid		All	0-10	9	<b>—</b>	0	0	0	0	0	0	-
99	Coal/Wood/NFF Liquid/NFF Solid		All A	10-100	35	2	0	0	0	0	0	0	2
25	Coal/Wood/NFF Liquid/NFF Solid		All	100-250	173	-	0	0	0	0	0	0	-
8	Residual Liquid FF		All A	0-10	က	159	6	10	33	37	42	47	20
8	Residual Liquid FF		All	10-100	37	304	09	91	124	33	184	49	7.1
82	Residual Liquid FF		Ŧ	100-250	172	63	2	8	12	19	17	27	20
83	Residual Liquid FF	•	All	>250	547	7	2	0	5	0	7	0	0
1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	TOTAL	1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1	Committee to the committee of the commit	,	1 B 1	5,268	516	618	. 703	834 A	1,219	1,452	2,597

Appendix A-2. Distribution of Model Process Heaters Between Fuel Switching Scenarios A, B, and C

	Model Paramete	Model Parameters (Capacity in MMBtu/hr)	ر ا الا مراجع الا الا مراجع المراجع ا	,		Known	wn	Assu	Assumed		Total	
Mode			Capacity	Avg	Final # of	• • •		Heaters w/o Capacity Data distributed into	Heaters w/o Capacity Data distributed into		·	
٩ ۲	Material	Combustor Type	Range	Capacity	Units	Case A	Case B	Model - Case A	Model - Case B	Case A	Case B	Case C
- ‹	Coal	Other	0-10	4	0	0	0	0	0	0	0	0
7	Coal	Other	10-100	54	0	0	0	0	0	0	0	0
က	Coal	Other	100-250	166	0	0	0	0	0	0	0	0
4	Coal	Other	>250	565	0	0	0	0	0	0	0	0
တ	Coal	Wall-fired/PC	0-10	7	0	0	0	0	0	0	0	0
9	Coal	Wall-fired/PC	10-100	22	0	0	0	0	0	0	0	0
_	Coal	Wall-fired/PC	100-250	186	0	0	0	0	0	0	0	0
80	Coal	Wall-fired/PC	>250	009	0	0	0	0	0	0	0	0
၈	Coal/Wood/NFF Liquid/NFF Solid	Ail	0-10	9	0	0	0	0	0	0	0	0
2	Coal/Wood/NFF Liquid/NFF Solid	All	10-100	35	0	0	0	0	0	0	0	0
=	Coal/Wood/NFF Liquid/NFF Solid	All	100-250	173	0	0	0	0	0	0	0	0
12	Coal/Wood/NFF Liquid/NFF Solid	All	>250	565	0	0	0	0	0	0	0	0
9	Residual Liquid FF	₩.	0-10	က	75	2	4	6	17		21	43
4	Residual Liquid FF	Ā	10-100	37	516	36	44	26	118	133	162	221
45	Residual Liquid FF	Ail	100-250	172	99	S	8	2	9	7	9	20
43	Residual Liquid FF	All	>250	547	17	0	6	0	က	0	12	2
47	Coal	Other	0-10	4	0	0	0	0	0	0	0	0
48	Coal	Other	10-100	54	0	0	0	0	0	0	0	0
49	Coal	Other	100-250	466	0	0	0	0	0	0	0	0
20	Coal	Other	>250	565	0	0	0	0	0	0	0	0
25	Coal	Wall-fired/PC	10-100	25	0	0	0	0	0	0	0	0
53	Coal	Wall-fired/PC	100-250	186	0	0	0	0	0	0	0	0
24	Coal	Wall-fired/PC	>250	909	0	0	0	0	. 0	0	0	0
22	Coal/Wood/NFF Liquid/NFF Solid	₹	0-10	9	0	0	0	0	0	0	0	0
99	Coal/Wood/NFF Liquid/NFF Solid	All	10-100	35	0	0	0	0	0	0	0	0
25	Coal/Wood/NFF Liquid/NFF Solid	ΑĒ	100-250	173	0	0	0	0	0	0	0	0
8	Residual Liquid FF	₽ F	0-10	3	80	-	-	ဗ	9	4	4	0
8	Residual Liquid FF	All	10-100	37	23	6	-	12	,	21	2	0
82	Residual Liquid FF	¥.	100-250	172	0	0	0	0	0	0	0	0
83	Residual Liquid FF	All	>250	547	0	0	0	0	0	0	0	0
STATE OF	设计的 TOTAL TOTAL TO THE SECOND TO THE SECOND	· · · · · · · · · · · · · · · · · · ·	10 10 10 10 10 10 10 10 10 10 10 10 10 1	7 Tg	∵202	. 53	.∻ 88 ∻	122 🐃 🛰	以下分位152 mecon	€.175 /∉	₹ 241	289

## Appendix A-3. Fuel Switching Costing Algorithsm

Total Capital Investment		TCI <sub>fs</sub> = total capital investment of fuel switching, \$ CE. = cost factor for first ewitching \$\xi\$/kw see
$TCI_{l_b} = (293) (CF_{l_5})(HI)$		1
CaseDescriptionCFsAGas @ combustion unit8.74BGas @ plant12.6	3	C <sub>ptpc</sub> = cost factor for piping, \$/foot pipc pipe = piping distance, feet TCL <sub>casc</sub> = capital invt for case C1, C2, C3, C4
C No gas: $TCI_{case C} = TCI_{case B} + (C_{pipe})(pipe)(\%_{case})$ $TCI_{case C} = TCI_{case C} + TCI_{case C} + TCI_{case C}$	3 + TCL <sub>case c4</sub>	$1  \text{C.}_{\text{case}}  c^{=}  \text{capital investment for case C}$ $\%_{\text{case}} = \text{percent of units in case}$
<u>Total Annual Cost</u>		delF = difference in fuel cost \$/yr
$TAC = dell^2 + EL + CR + All_{SO2} + CAP$		802 = = = 1
$delF = (CF_g - CF_{corr})(H1)$ (0)		CF <sub>g</sub> = cost factor for gas, \$/MMBtu CF <sub>corr</sub> = cost factor for coal or resd., \$/MMBtu HI = heat input, MMBtu/hr 0 = hours of operation
$\text{EL} = \left[ \frac{111}{1 - \text{ELF}} - 111 \right] \left[ \theta \right] \left[ CF_{\star} \right]$		EL = efficiency loss, \$/yr HI = heat input, MMBtu/hr 0 = hours of operation ELF = efficiency loss factor CF <sub>g</sub> = cost factor for gas, \$MMBtu
$CR = (TC1)(CRF_{ls})$		CRF <sub>fs</sub> = capital recovery factor fuel switching
$CFR_{b} = \frac{\left[i(1+i)^{n}\right]}{\left[(1+i)^{n}-1\right]}$		i = interest rate, fraction n = life of equipment, yrs

### Appendix A-4. Fuel Switching Input Parameters and Values

Parincia	<u> विह्हालग्राहरू</u>	Asine	. Light
CF-A, coal	Cost factor for scenario A, coal	8.74	\$/kw
CF-B, coal	Cost factor for scenario B, coal	12.63	\$/kw
CF-A, oil	Cost factor for scenario A, oil	6.05	\$/kw
CF-B, oil	Cost factor for scenario B, oil	9.91	\$/kw
CF-C1	Cost factor for case C1	125	\$/foot pipe
CF-C2	Cost factor for case C2	25	\$/foot pipe
CF-C3	Cost factor for case C3	25	\$/foot pipe
Cost-gas	Cost of gas per volume	3.59	\$/Mscf
HV-gas	Heating value of gas	1,020	Btu/scf
CFg	Cost of gas per MMBtu	3.52	\$/MMBtu
Cost-coal	Cost of coal per mass	35.72	\$/metric ton
HV-coal	Heating value of coal	12,000	Btu/lb
CFc	Cost of coal per MMBtu	1.35	\$/MMBtu
Cfdo	Cost factor for distillate oil	5.10	\$/MMBtu
Cfro	Cost factor for residual oil	2.90	\$/MMBtu
i	Interest rate	0.07	%
n	Life of equipment	20	years
CRF	Capital recovery factor	0.09439293	-
ELF	Efficiency loss	0.05	
theta	Hours of operation a year	8,400	hours/year

Appendix A-5. Fuel Switching -- Components of Capital Cost

	Sy	System	Scenario	ario		Sost Breakdo	Cost Breakdowns (\$/kw) for Each Site <sup>b</sup>	or Each Site	q
	\$ P\$			4 28 6	Boiler 1	Boiler 2	Boiler 3	Boiler 4	Boiler 5
Capital Cost Components	Gas system	Boiler system	∢	m	(Table 9) <sup>c</sup>	(Table 10) <sup>c</sup>	(Table 11) <sup>c</sup>	(Table 12) <sup>c</sup>	(Table 13) <sup>c</sup>
Electrical gas meter house				×			90		
Regulator house extension	×			×		0.13	-		
Mechanical erection pkg	×			×		2.9			
Insulation	×		•			0.62	9.0		
Platforms and supports	×			×		0.17			
Gas house extension	×			×	0.5				
Conduit and Cable	×			×	2	0.16			
Gas piping	×						4.8		4.04
Gas, vent purge piping	×				3.2				
U.G. Piping and tap	×			×			0.3		
Grating and pipe supports	×			×	0.3				
Meters, regulators, and scrubber	×			×		:	2.6		
Purging	×			×		0.01			
Electrical boiler		×	×	×		1.5	2		0.28
Fans, ducts, temp. probes		×	×	×		0.1			
Mechanical fabrication pkg		×	×	×		0.72			0.24
Superheater upgrading		×	×	×		2.31			
Gas ignition control system		×	×	×	3.5				
Boiler controls		×	×	×					
Boiler modifications		×	×	×	3.2		2.1		4.04
Burner managment system ctrol vlv		×	×	×					
Fans		×	×	×					
Valves, instruments, controls		×	×	×	3		0.4		
Ignitor modifications		×	×	×		0.57			
Administrative			×	×					
Design			×	×					
Engineering			×	×					0.5
Overhead			×	×					0.2
Project Management			×	×	0.5	0.95	0.5		
Test, start-up, calibration			×	×		0.21	0.1		
Training			×	×					
Transportation			×	×		0.01			
Vendor representative			×	×	0.1	0.88	0.5		
building and excavation							0.0		

a Scenario A = Boiler already has gas as a startup or backup
 Scenario B = Plant uses gas as a fuel but boiler does not
 b Data taken from Reference 8.
 c Data for each boiler was taken from the noted Table in Reference 8.

Scenario A

	Sys	tem	1 Tre .	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	Cost Break	kdowns (\$/kw	) for Each Si	te <sup>a</sup>	
Capital Cost Components	Gas system	Boiler system	Boiler 1 (Table 9) <sup>b</sup>	Boiler 2 (Table 10) <sup>b</sup>	Boiler 3 (Table 11) <sup>b</sup>	Boiler 4 (Table 12) <sup>b</sup>	Boiler 5 (Table 13) <sup>b</sup>	Average Cost	Average Cost (in 1997 Dollars)
Electrical boiler		x		1.5	2		0.28		
Superheater upgrading		×		2.31	-				
Gas ignition control system		×	3.5						
Boiler controls		×		·		-			
Boiler modifications		×	32		2.1		4.04		
Burner managment system		×	Ì						
Valves, instruments, controls		×	3		0.4				
Ignitor modifications		х		0.57					
Fans, ducts, temp, probes		×		01					
Mechanical fabrication pkg		×		0.72		-	0.24		
Purging	×			0.01		-			
Subtotal			9.7	5.21	4.5		4.56	5,99	7.24
Administrative									
Design			·						
Engineering							0.5		
Overhead							02		
Project Management			0.5	0 95	0.5				
Test, start-up, calibration				0.21	0 1				
Training									
Transportation			,	0 0 1					
Vendor representative			01	0 88	0.5				
Building and excavation					0.5				
Subtotal			0.6	2.05	1.6		0.7	1.24	1.50
Total								7.23	8.74

### Scenario B

	Sys	tem			Cost Break	(downs (\$/kw	ı) for Each Si	te*	PETER STATE
Capital Cost Components	Gas system	Boiler system	Boiler 1 (Table 9) <sup>b</sup>	Boiler 2 (Table 10) <sup>b</sup>	Boiler 3 (Table 11) <sup>b</sup>	Boiler 4 (Table 12) <sup>b</sup>	Boiler 5 (Table 13) <sup>b</sup>	Average Cost	Average Cost (in 1997 Dollars)
Electrical gas meter house	×		(1111111)	1.22.2	0.6	111210 127	1.1111		( 100. Donalo)
Regulator house extension	x			0.13					
Mechanical erection pkg	x		•	2.9					
Platforms and supports	x		l	0.17					
Gas house extension			0.5						
Conduit and Cable	- <del>x</del> x		2	0.16				*	
U.G. Piping and tap	X				0.3				
Grating and pipe supports	x	-	03	ŀ	3.0				
Meters, regulators, and scrubber	x	-			26				
Purging	×			0.01					
Subtotal			2.8	3.37	3.5			3.22	3.90
Electrical boiler		x		1.5	2		0.28		0.00
Fans, ducts, temp probes		×		0.1	-		0.20		
Mechanical fabrication pkg		×		0.72			0 24		
Superheater upgrading		x		2 31			02-		
Gas ignition control system			3.5						
Boiler controls	1	x							
Boiler modifications		x	3.2		2.1		4.04		
Burner managment system	ļ	×	5.2		2		4.04		
Fans		x							
Valves, instruments, controls		×	3		0.4				
Ignitor modifications		x		0 57	9.4				
Subtotal			9.7	5.2	4.5		4.56	5.99	7.24
Administrative				V.E	4.0		7.30	0.00	7.47
Design									
Engineering							0.5		
Overhead							02		
Preject Management	İ		0.5	0.95	0.5		- 02		-
Test, start-up, calibration			5.5	0.21	0.1				
Training	į			V.21	· · · · · ·	-	•		
Transportation				0.01			- 1	İ	
Vendor representative	ł		0.1	0.88	0.5	- •	-		
Building and excavation	1		J	5.55	0.5		-		-
Subtotal			0.6	2.05	1.6		0.7	1.24	1,50
Total							<u> </u>		
iotai							i	10.45	12.63

a Data taken from reference 8

b Data for each boiler was taken from the noted Table in Reference 8

1000						Total (	Total Capital Investment (\$)	ent (\$)	Total	Total Annual Costs (\$/yr)	\$/yr)
								,			
Model	at Material	Combustor Type	Capacity Range (MMBtu/hr)	No. of Boilers	No. of Heaters	Boiler Fuel Switching	Heater Fuel Switching	Total Fuel Switching	Boller Fuel Switching	Heater Fuel Switching	Total Fuel Switching
_	Сол	Other	0-10	83	0	17,216,016	0	17,216,016	8,216,675	0	8,216,675
2	Coal	Other	10-100	919	0	262,258,854	0	262,258,854	1,003,403,469	0	1,003,403,469
е е	Coal	Other	100-250	509	0	336,553,198	0	336,553,198	1,697,833,339	0	1,697,833,339
4	Coal	Other	>250	204	0	422,992,860	0	422,992,860	2,306,934,969	0	2,306,934,969
S	Coal	Wall-fired/PC	0-10	12	0	1,277,558	0	1,277,558	598,902	0	598,902
9	Coal	Wall-fired/PC	10-100	86	0	23,237,489	0	23,237,489	112,456,085	0	112,456,085
~	Coal	Wall-fired/PC	100-250	212	0	146,998,419	0	146,998,419	791,860,501	0	791,860,501
∞	Coal	Wall-fired/PC	>250	291	0	591,571,540	.0	591,571,540	3,498,591,792	0	3,498,591,792
6	Coal/Wood/NFF Liquid/NFF Solid	¥	0-10	7	0	1,604,483	0	1,604,483	978,885	0	978,885
9	Coal/Wood/NFF Liquid/NFF Solid	₹	10-100	29	0	22,034,050	0	22,034,050	48,134,768	0	48,134,768
Ξ	Coal/Wood/NFF Liquid/NFF Solid	¥	100-250	81	0	11,716,403	0	11,716,403	62,572,304	0	62,572,304
12	Coal/Wood/NFF Liquid/NFF Solid	₹	>250	1.1	0	146,345,808	0	146,345,808	871,679,071	0	170,679,178
9	Residual Liquid FF	₹	0-10	477	75	89,908,618	11,400,818	101,309,435	18,207,874	5,515,993	23,723,867
4	Residual Liquid FF	¥	10-100	1,154	516	321,616,111	120,083,824	441,699,935	317,534,242	387,544,277	705,078,519
45	Residual Liquid FF	₹	100-250	264	99	145,060,286	45,653,139	190,713,425	319,682,287	228,243,474	547,925,761
43	Residual Liquid FF	₽	>250	141	17	210,390,295	35,621,095	246,011,389	539,554,206	186,781,423	726,335,629
47	Coal	Other	0-10	36	0	9,389,755	0	9,389,755	1,839,340	0	1,839,340
48	Coal	Other	10-100	20	0	15,002,895	0	15,002,895	26,915,780	0	26,915,780
49	Coal	Other	100-250	53	0	39,839,259	0	39,839,259	94,862,605	0	94,862,605
જ	Coal	Other	>250		0	10,085,356	0	10,085,356	27,567,428	0	27,567,428
25	Coal	Wall-fired/PC	10-100	32	0	6,135,600	0	6,135,600	12,897,842	0	12,897,842
53	Coal	Wall-fired/PC	100-250	6	0	7,077,388	0	7,077,388	11,873,271	0	11,873,271
54	Coal	Wall-fired/PC	>250	15	0	18,715,031	0	18,715,031	62,518,961	0	62,518,961
55	Coal/Wood/NFF Liquid/NFF Solid	¥ A	0-10	-	0	276,475	0	276,475	62,029	0	62,029
29	Coal/Wood/NFF Liquid/NFF Solid	¥	10-100	8	0	698,486	0	698,486	534, 196	0	534, 196
25	Coal/Wood/NFF Liquid/NFF Solid	₹	100-250	<del></del>	0	748,155	0	748,155	1,228,670	0	1,228,670
8	Residual Liquid FF	₽ F	0-10	159	8	18,601,502	75,137	18,676,639	4,957,869	481,913	5,439,782
8	Residual Liquid FF	₹	10-100	304	23	42,545,168	2,276,252	44,821,420	79,895,059	17,051,225	96,946,284
82	Residual Liquid FF	<b>A</b>	100-250	63	0	33,227,462	0	33,227,462	76,183,650	0	76,183,650
83	Residual Liquid FF	All	>250	7	0	6,787,477	0	6,787,477	26,540,852	, 0	26,540,852
*	TOTAL - CALINGTON OF THE STATE	Charles American	The state of the second of the second	5,268	. 705	2,959,911,994	215,110,265	3,175,022,259	12,026,119,921	825,618,306	12,851,738,227

		Mortel Parameters	でなどの意思をなる!	ここ のの様 変の数	- 2	Total	i Ni mbox	_									,
L		1	10 yr 6	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1		-	i reusinuen	1	Capital INVES	Capital Investment for Each Scenario	ano	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1		Total Annual Cost	ual Cost		
Mode	76		Capacity	Average	No. Of	- 44 - 3 - 4	學					Additional Final		Capital	Capital	Capital	
Ž	_	Combustor Type	(MMBlunc)	(MMBtu/hr)	_	Case A C		Case C Case A	e A Case B	Case C	Total	Cost	Efficiency Loss	Case A	Case B	recovery - Case C	Total
-	Coat	Ottner	0.10	4	83		13 6	64 54,851	198,161	16,963,004	17,216 016	6,004,844	512,662	5 178	18,705	1,675,287	8,216,675
N i	Coal	Other	10.100	₹.	01.0	192	361	366 26,513772	1772 72,225,08	163,520,001	262,258,654	900,981,751	76,921,071	2,502,713	6.817,537	16, 180, 397	1,003,403,469
۰ رد	Coal	Other	100-250	166	505	- 14	210 1	185 48 281 785	785 129,205,641	41 159,065,772	336,553,198	1,534,556,062	131,012,305	4,557 459	12,196,098	15,511,414	1,697,833,339
4 (	Coal	Officer	>250	. 595	504	20	32	122 72,343,165	3,165 - 66,906,667	7 283,743,026	422,992,860	2,088,394,720	178,296,129	6,828,683	6,315,516	27,099,921	2,306,934,969
۰ ۵	Coal	Wall fred/PC	0.10	~i	12	,	, 2	5 12 292	92 35,526	1,229,740	1,277,558	435,722	37,200	1,160	3,353	121,467	598,902
φ	Codi	Wall fred PC	10-100	. 22	86	85	41.	26 8,514,727	727 2.953,071	11,769,692	23,237,489	101,554,932	8,670,225	603,730	278.749	1,148 449	112,456.085
_	Coal	Wall fred PC	100-250	186	212	89	6	63 32,179,883	1,883 56,123,717	17 58,694,818	146,998,419	716,633,892	61,182,423	3,037,553	5,297,682	5,708,950	791,860,501
œ ·	Coal	Wall bred PC	>250	009	281	114	76 1	100 175,915,740	5.740 169,474,889	89 246,180,912	591,571,540	3,171,652,278	270,778,948	16,605,201	15,997,231	23,558 135	3,498,591,792
<b>a</b>	COAL/WOOD/NFF LIQUICENFF SOILD	All.	0-10	9	7		 -	0 9	25,904	1,578,579	1,604,483	759,196	64,816		2,445	152,427	978.885
2	Coal/Wood/NFF Liquid/NFF Solid	All .	10-100	32	29	 &	4.	55 727,854	394 525,932	20,780,224	22,034,050	42,394,931	3,619,456	68,708	49,644	2,002,029	48 134 768
=	Coal/Wood/NFF Liquid/NFF Solid	All	100-250	173	81	4	e	4 1,876,328	.328 6,100,749	9 3,739,326	11,716,403	56,628,434	4,834,637	177,112	575,868	356,253	62,572,304
2	Coal/Wood/NFF Liquid/NFF Solid	AH	>520	265	11	35	20	26 46,048 836	1836 40,785,189	9 59,511,783	146,345,808	790,365,776	67,477,262	4.346,684	3,849,833	5,639,515	871,679,071
4	Residual Liquid FF	Y Y	0.10		477	 97		347 256,877	377 710,048	88,941,693	89,908,618	7,398,404	2,210,729	24,247	67,023	8,507,471	18,207,874
4	Residual Liquid FF	IV	10-100	37	1,154	129	210 . 8:	815 8,485,270	22,516,401	11 290,614,441	321,616,111	220,800,625	65,977,776	800,949	2,125,389	27,829,503	317,534,242
4.2	Residual Liquid FF	¥	100-250	172	564			108 21,697,976	.976 42,420,67	71 80,941,639	145,060,286	235,518,361	70,375,605	2,048,135	4,004,211	7,735,974	319,682,287
£ i	Residual Liquid FF	Als.	>520	547	- 4	4	36	58 42,584,662	.662 62,411,813	13 105,393,820	210,390,295	400,031,197	119,533,640	4,019,691	5,691,234	10,078,145	539,554,206
÷ '	Coal	Other	0-10	4	98	o		36 0	0	9,389,755	9,389,755	742,452	221,853	ວ		875,034	1,839,340
<b>4</b>	Coal	Other	10-100	<b>2</b> 5	20	م		478,616	7,447,811	1 7,076,468	15,002,895	19,637,024	5,867,770	45,178	703,021	662,787	26,915,780
49	Coal	Other	100-250	466	58	 ო	16	10 2,661,732	732 21,799,809	15,377,718	39,839,259	70,146,309	20,960,527	251,249	2,057,748	1,446,773	94,862,605
3	Coal	Olher	>520	999	~	4	 o	3,505,415	415 0	6,579,940	10,085,356	20,494,652	6,124,039	330,886		617,851	27,567,428
3 8	Coal	Wall-bred/PC	10.100		35	٠	23 E	5 461,902	3,783,015		6,135,600	9,485,821	2,834,473	43,600	357,090	176,858	12.897,842
3	Coal	Wall-tried/PC	100-250	186	G.		 O	0		7,077,388	7,077,388	8,631,010	2,579,045	0	0	663,216	11,873,271
<b>.</b>	Cost	Wall-lired/PC	>520	009	5	2		12,763,080		5,951,951	18,715,031	46,778,256	13,977,883	1,204,744	•	828,078	62,518,961
8 8	Coal/Wood/NFF LiquidNFF Solid	₹ .	9	O	_	 o	 o	э 	0	276,475	276,475	30,936	9,244	0	0	24,849	62.029
8 (	Coar,Wood/Nr Liquid/Nr Solid	₽.	10.100	98	8			o 	0	698,486	698,486	360,914	107,845	0	0	65,436	534,196
à	Coal/Wood/NFF Liquid/NFF Solid	₹ .	100-250	173	_	o	0	-	0	748,155	748,155	891,974	266,532	a	0	70,163	1,228,670
3 3	Residual Liquid FF	₹	0.10	ო	159		7 74	70 223,823	123 407,362	17,970,316	18,601,502	2,473,256	739,038	21,127	38,452	1,685,995	4,957,869
<b>5</b> 6	Residual Liquid FF	TV	901-01	37	30 <del>.</del>	<b>2</b> 8	•	1 12,084,101	,101 5,278,389	9 25,182,678	42,545,168	58,443,490	17,463,590	1,140,654	498,243	2,349,083	79,895,059
82	Residual Liquid FF	₹ .	100-250	172	63	17		0 5,054,851	851 13,247,888	8 14,924,722	33,227,462	56,255,676	16,809,845	477,142	1,250,507	1,390,480	76,183,650
2	Residual Liquid FF	AJI	>250	547	,	7	0 0	6,787,477	477 0	0	6,787,477	19,941,432	5,958,730	640,690		0	26,540,852
<u>``</u>	TOTAL: 24 18 18 18 18	And the second	のはいい		5,268	1,219	1,452 2,597	97 529,515,055	5,055 724,583,734	_	1,705,813,206 2,959,911,994	10.588.424.330 1.155.425.598 49.982.475	1.155.425.598	49 982 478	15	163 891 940	68 395 579 163 891 940 12 026 119 921
				The second secon						71					_13	T	

Part   Part	L_		Model Parameters 👵	The second second	· 1000000000000000000000000000000000000		Total	Total Number		J. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1.	Capital Ir	Capital Investment	San San Jane	, , , , , , , , , , , , , , , , , , ,		Ann	Annual Cost		
Column	Mod				Average Capacity	11 ( 7.30								Additional	Efficiency	Capital Recovery	Capital Recovery -	Capital Recovery -	
Column   C	2		Combustor 1)		(MMBtumr)	1			o ase	Case A	Case B	Case C	Total	Fuel Cost	5901	Case A	case p	Case C	Total
Couli Convex Con	-	Coal	Other	0.10	4	Φ	:			:	;	,	!	;		;	:		1
Coal Otton Original 166 0	7	Coal	Other	10.100	<u>2</u>	0	:			;	;	:	1	:	:	:	:	:	;
Coult Coult Would Marketing PO - 0.10 - 0.2 - 0 0 0 0 0 0	6	Coal	Other	100-250	166	0	;			,	:	:	1	:		;	:	,	1
Coulting   Walkbroad   Coulting   Walkbroad   Coulting   Walkbroad   Coulting   Walkbroad   Coulting   Walkbroad   Coulting   Walkbroad   Coulting   Walkbroad   Coulting   Coulting   Walkbroad   Coulting   Coulting   Walkbroad   Coulting	4	Coal	Other	>250	599	0	;		:	:	;	:	!	;		;	;	:	1
Column	3	Coal	Wall-fired/PC		٦,	0	;		:	;	;		;	;	;	;	:	:	ı
Columnosida   Columnosida	9	Coal	Wall-fired/P(		25	0	:		:	:	;	;		1	;	;	;	:	ı
Coality Coal	~	Coal	Wall-fired/PC	•	186	0	;	:	;	;	;	;	1	;	;	;	;	;	:
Coard/Moodroff Equatoff Solid   Ali	æ	Coal	Wall-fired/PC		009	0	:	:	:	:	:	:	ì	į	:	;	;	:	ŀ
Coard-Monosome File and Mail   10-100   35   10   11-10	on.	COAI/WOOD/NFF LIQUID/NFF SOIL		01-0	9	0	:	;	;		:	:	;	1	:	;	;	:	:
Coal/MotorNFF Sulu         All         100-260         173         0         2.21         2.277 895         1 1,400-818         4077 864         3-81-37         7770         2.246         10.90-75           Coal/MotorNFF LquarMFF Sulu         All         1 0.0         37         616         13         162         221         12.572.01         22.204 809         8.306.99         10.006.818         4.077.864         3-81-37         7770         2.246         10.002         37         61         1         4.0         20         2.207.04         2.2204 809         8.306.99         10.008.83         3.465.17.59         2.04.30.37         3.465.17.59         2.04.30.34         3.11.00.24         3.007.24         3	2	Coal/Wood/NFF Liquid/NFF Solic		10-100	35	0		;	;		:	;	;	:	1	:	:	;	ı
Coal-Monotoning F and   Coal	=	1 Coal/Wood/NFF Liquid/NFF Solic		100-250	173	0	:	:	:	;	;	;	;	:	:	1	;	:	ı
Page-state   Pag	12	2 COSINVOOUNFF LIQUIUNFF SUIL		>250	595	0	1	:	:	;	;	;	ı	;		;	:		;
Resolution In Terms         All         10-100         37         616         13         12, 27, 20, 1809         63, 30, 699         17, 50, 683, 824         17, 610, 634         48, 517, 509         246, 517, 509	5	) Residual Liquid FF	- All	0.10	en	7.5	=	21	43	82,312	237,895	11 080,611	11,400,818	4,077,864	348,147	7,770	22.456	1,059,757	5,515,993
Residual Liquid FF Aii 100-250 172 66 7 7 410 20 2907043 175.013 10 206.303.483 17.013.104 274.04 277.017 167.3276 Coal Coal Color Coal Coal Color Coal Color Coal Color Coal Color Coal Color Coal Color Coal Color Coal Color Coal Color Coal Color Coal Color Coal Color Coal Color Coal Color Coal Color Coal Color Coal Color Coal Coal Color Coal Coal Color Coal Color Coal Color Coal Color Coal Color Coal Coal Color Coal Coal Color Coal Coal Color Coal Coal Color Coal Coal Coal Coal Coal Coal Coal Coal	4	1 Residual Liquid FF	F	10.100	37	516	133	162			22,204,609	85,306,999	120,083,824	346,517,509	29,583,838	1,186,709	2,085,977	8,160,244	387,544,277
Residual Liquid FF         All         250         647         77         0         12         5         0         23823.644         11/97/560         35.621,065         166,890,627         14,425.675         0         2248,774         1125,347           Coal         Other         0.10         4         0	42	2 Residual Liquid FF	F	100-250	172	99	7	40			25,205,459	17,540,638	45,653,139	206,303,483	17,613,104	274,404	2,379,217	1,673,266	228,243,474
Coal         Other         0-10         4         0 <th>£.</th> <th>3 Residual Liquid FF</th> <th>All</th> <th>&gt;250</th> <th>547</th> <th>17</th> <th></th> <th>1.2</th> <th>ç,</th> <th></th> <th>23,823,544</th> <th>11,797,550</th> <th>35,621,095</th> <th>168,980,627</th> <th>14,426,675</th> <th>0</th> <th>2,248,774</th> <th>1,125,347</th> <th>186,781,423</th>	£.	3 Residual Liquid FF	All	>250	547	17		1.2	ç,		23,823,544	11,797,550	35,621,095	168,980,627	14,426,675	0	2,248,774	1,125,347	186,781,423
Coal	4	Coal	Other	01-10	4	0	;	,	;	;	:		;	ı	:	:	;	:	:
Coal         Other         250         466         0 <th>æ</th> <th>9 Coal</th> <th>Other</th> <th>10-100</th> <th>2</th> <th>0</th> <th>;</th> <th>ı</th> <th>;</th> <th>. ,</th> <th>;</th> <th></th> <th>ı</th> <th>ı</th> <th>;</th> <th>;</th> <th>;</th> <th>:</th> <th></th>	æ	9 Coal	Other	10-100	2	0	;	ı	;	. ,	;		ı	ı	;	;	;	:	
Coal         Wall-finedPC         10-100         57         0  <	49	Coat	Other	100-250	466	0		:	:	;	:	!	1	;	;	1	:	;	•
Coal         Wall-fined/PC         10-100         57         0	જ	Coal	Other	>250	999	0	:	;	;	:	:		,	;	;	;	:	:	1
Coal         Wall-fred/PC         100-260         186         0	25	2 Coal	Wall-fired/PC		25	0	;		:		;	;	;	;	;	;	;	;	ł
CoalWoodNFF LiquidNFF Solid All 10-100 35 0	53	3 Coal	Wall-fired/PR		186	0	;	:	;		;		1	;	;	;	;	;	;
CoalWood/NFF Liquid/NFF Solid All 10-100 35 0	Ÿ	t Coal	Wall-fired/PC	<b>-</b>	009	0		;	;	:	:	1	1	1	;	:	:	;	
CoalWoodNFF LiquidNFF Solid All 10-0250 173 0	55	S Coal/Wood/NFF Liquid/NFF Solic		0.10	9	0	1	:	1	1	;	:	1	;	:	;	;	:	1
Coal/Mood/NFF Liquid/NFF Solid         All         100-250         173         0	જુ	•		10.100	35	0		:	:		;	:	!	;	:	;	;	;	1
Residual Liquid FF         All         0-10         3         8         4         4         0         30,730         44,407         0         75,137         437,472         37,349         2,901         4,192         0           Residual Liquid FF         All         10-100         37         23         21         2         0         1,961,332         314,920         0         2,276,252         15,512,028         1,324,335         185,136         29,726         0           Residual Liquid FF         All         >250         547         0         37,133,034         125,725,797         125,110,268         141,828,863         67,803,344         14,600,301         67,803,344         14,000,301         17,018,614	25			100-250	173	0		:	;	:		:	;	;		:	;	:	1
Residual Liquid FF All 10-100 37 23 21 2 0 1:061,332 314,020 0 2.276,252 15,512,028 1.324,335 185,136 29,726 0 Residual Liquid FF All 250 547 0 175 20 17,631,034 125,725,797 215,110,265 741,828,983 63,333,447 1,666,920 6,780,341 12,018,614	8	•	A	0.10	<sub>6</sub> 0	89	4	4	0	30,730	44,407	0	75,137	437,472	37,349	2,901	4,192	0	481,913
Residual Liquid FF All 100-250 172 0 All 289 173 10 All 289 175 241 289 17.853.433 71.831,034 125.725.797 215.110.265 741.828.983 63.333.447 1.666.920 6.780.341 12.018.614	<u>=</u>	•	All	10-100	37	23	21	7	0	1,961,332	314,920	0	2,276,252	15,512,028	1,324,335	185,136	29,726	0	17,051,225
Residual Liquid FF All >250 547 0	82	•	. All	100-250	172	0	;	1	:	:	I	:	;	:	;	1	;	:	:
125.725.797 215,110.286 74,828,983 63,333,447 1,686,920 6,789,341 12,018,614	83	Г	All	>250	547	٥	:	;	:			-			-	-	***	*-	:
	r	TOTAL	聖書は養養ないない	能力と大変な		_	- 50			7.553.433				741.828.983	63,333,447	1.656.920	6.780.341	12.018.614	825.618.306

Appendix A-9. Capital Investment and Annual Cost for All Process Heaters in Applicable Models for Fuel Switching

### Appendix A-10. Breakdown of Case C Costs for Boilers

Щ	·	Model Parameters		*			N N	Number of Case C Bollers	Hers				Capita	Capital Cost		
		\$.D		-		% population	£	z	10	-	62 500 00	112 000	1 320	< = \$ per unit		\$/model
Model	Material	Combustor Type	Capacity Range (MMBturfir)	Average Capacity (MMBludhr)	76.0 Cales	Total	C1 (500 feet)	C2 (1 mile)	C3 (10 miles)	C4 (No Pipe)	C1 (500 feet)	C2 (1 mle)	C3 (10 miles)	ang C4 (No	C4 (No Pipe) -	1
_	Coal	Other	010	7	23	3		1	ė		200 806	7 124 934	8 482 065	332 315	4115	16 021 345
2	Con	Other	10-100	 Z	919	366	20	200	37	•	1,143 240	40 563 999	48 290 475	313 657	1 14/ 472	91 145,186
n	Coul	Odker	100-250	99	ş	185	э.	55	61	2	578.409	20,522 880	24 432,000	523 272	875 806	46,501,817
<del>-</del>	Com	. Other	>520	265	20.	122	a	102	12	-	381,250	13 527,360	16, 104 000	983,251	1 199 500	31,212,176
<u>.,,</u>	Coal	Wall fred/PC	01.0	~	12	'n	3	•	0	0	15,000	532,224	633,600	286 369	13 /46	1 194,570
9	Coal	Wall fund/PC	10-100		8	56	-	22	m	0	60,208	2 845 920	3 368 000	373 014	95 740	6,409,868
_	Court	WalthedPC	100-250	98	212	63	c	53	9	-	196.566	6.974 474	8 302 945	569.702	956 349	15 832,333
-	Coa	Wall fred/PC	×250	909	291	99	£	2	01	-	313,064	11 107 995	13 223 803	1,322,232	1 324 616	25,969,478
<b>"</b>	COalWood/NFF LIQUATMER SUILD	₹ .	9. 0.	 •	~	9	0	'n	-	0	18,229	646,800	270 000	262 698	15 324	1,450,353
2	COMMODANE LIQUADNEE SOLD	₹	10-100	 g	29	55	c	9	ç	-	171,307	6,078 240	7 236,000	484 496	262 267	13,751,139
=	COMMODINE ENGINEE SOND	₹ .	100-250	£71	2	•	0	•	0	9	13,235	469 609	559 058	309.138	13 093	1 054,996
~	COAFWOODINF ENGINEERIF SUM		^220	295	"	26	-	22	r	0	80.208	2,845,920	3,388 000	271,088	625.69	6 383,708
2	Residual Exquid FF	₹ .	91-6		11.1	347	13	292	şç Ş	~	1.084,949	38 495 711	45 828,228	155, 163	538 770	85,947,658
=	Residual Liquid FF	₹	10-100	37	25	815	7	685	83	40	2.547,015	90,372,172	107 585 919	419,755	3 421 191	203,926 298
7	Residual Liquid FF	7	100 250	221	<b>564</b>	108	ş	16	=	-	337.174	11,963,470	14 242 226	974,932	1 051 909	27,594,779
7	Residual Liquid FF	**************************************	×250		Ξ	58	c	67	9	_	180,584	6,407,410	7 627,869	542 856	313 700	14 529,562
7	Con	Other	0-10	•	95	36	~	oc .	7	*0	112,500	3,991 680	4 752,000	332 315	119 634	8.975,814
₽	Coal	Ottro	201-01	<b>3</b>	0.	18	-	15	2	0.2	54,688	1,940,400	2 310,000	313 657	54 890	4,359,977
₽	Coal	Other	100-250	- · 99	82	01	90	<b>89</b>	-	0.1	30.208	1,071,840	1,276,000	523 272	50 583	2 428,631
S :	•	Office	×250	265	~	•	0.5	n .	*0	400	10.938	386,080	462 000	983 251	34 414	895,431
25		Wallfred/PC	5 5	3	35	'n	0.2	•	50	90 0	14 286	506,880	603,429	373 014	17 052	1,141,646
3	Coal	WalthedribC	100-250	98	o,	<sub>6</sub>	0.5	•	<u>-</u>	-0	28,125	997,920	1.188 000	569 702	51.273	2,265,318
Š		Wall-fued/PC	^520	9	ō.	0	0.2	e	03	0 03	9.375	332,640	396 000	1,322,232	39 667	777,682
33	-	₹	0.0	•	-	-	-0	<u>-</u>	10	000	3,125	110 880	132,000	1,322,232	13 222	259,227
Š		T V	10-100	8	2	~	10	~	20	0 02	6.250	221,760	264 000	262,698	5.254	497,264
23		. ₹	100-250	22	-	_	0.1	-	10	100	3,125	110 860	132 000	484 496	4 645	250,850
3	•	₹	2		159	70	•	. 69	1	-	219,210	7,777,906	9 259 412	155,183	108 856	17,365,384
<b>5</b>		T.	5 5	75	ğ	1.2	7	. 65	,	-	220,707	7,831,040	9 322 667	419 755	296 457	17,670,871
3 3	•	₹ .	100-250	172	63	20	-	- 12	7	0.2	62.171	2,205 928	2 626 105	974.932	193 560	5,088,165
8	Residual Jupout FF	Au	>250	547	,	0	0	0	0	0	0	0	•	•	0	0
45	roral	Market and the Control of the Contro	我主題		6.268	₹. 2,597	\$ <u>.</u>	> 2,182	260	36	8,115,952	287,966,953	342.817.801	16.160.693	12 000 821	650 901 527

L		Model P	Model Parameters . 527.54.	在一時間門一種 "	はは			,	Case C Boilers					Capital Cost		,
	-	7. X.		7.7	27 28 88		% population	5	84	10	-	62 500	132,000	1.320,000	e = \$ per unit	\$/model
Model No.	Material Material		Combustor Type	Capacity Range (MMBlu/hr)	rerage apacity ABtu/hr)	No. of Units	Total	C1 (500 feet)	C2 (1 mile)	C3 (10 miles)	C4( No Pipe)	C1 (500 feet)	C2 (1 mile)	C3 (10 miles)	C4 (No Pipe) Add on control	Total
_	Coul		Other	0.10	4	0		:	:	1	:		;			1
8	Coal		Other	10-100	2	0	;	1	:		:	;	;		;	;
က	Coat	-	Other	100.250	166	0	;	;			;	;	;	;	!	\$
4	Coal		Other	>250	565	၁	;	;			;	:	:	,		;
G	Coal		Wall-fired/PC	0-10	2	0	;	;	;	;	;	:	:	·	:	;
9	Coal	•	Wall-fred/PC	10-100	25	0	:	1		1	;	;	:		:	;
۷	Coal		Wall-fired/PC	100-250	186	0	:	1	:	}	ł	;	1		;	1
<b>6</b> 0	Coat		Wall-fired/PC	>250	009	0	;	;	:	- ·	:	;	ï			1
G	Coal/Wood/NFF Liquid/NFF Solid		All	0-10	 	0	;	;	;	;	i	:	;	:	1	;
2	CoalWood/NFF Liquid:NFF Solid		¥	10-100	32	0	:	;			1		;	:	1	;
Ξ	COSIMOOUNFF LIQUIDNFF SOND		¥	100-250	173	0	;	;	;	1	1		;		;	1
12	CoalMoodNFF LiquidNFF Solid		₹	>250	999	0	:	1	;	;	:	;	;	,	;	;
6	Residual Liquid FF	•-	₩	0-10		75		N.	36	4	0	133,929	4,752,000	5,657,143	66,507	10,609,578
4	Residual Liquid FF		Æ	10-100	37	516	221		186	22	2	691,071	24,520,320	20,190,857	928,258	55,330,507
42	Rosidual Liquid FF		Ψ	100-250	172	99	50	-	11	8	0	61,875	2,195,424	2,613,600	193,037	5,063,936
43	Residual Liquid FF		₹	>250	547	-2	5	0	4	<del>-</del>	0	16,346	579,968	690,462	28,396	1,315,191
47	Coal		Other	0.10	₹.	0	ï	;	;	1	;	<i>-</i>	:	;	1	1
48	Coal	•	Other	10-100	Z.	0	;	:	;	1	;	;	:	;	;	1
48	Coal		Other	100-250	466	0	·	;	:	;	:	:	1	;	;	1
ß	Coat		Other	>250	. 265	0	;	1		;	:	;	1	:	,	1
25	Coal		Wall-fired/PC	10-100	29	0	;	ı	;	;	1	;	1	:	;	1
23	Coat	_ •	Wall-fired/PC	100-250	186	0	;	:		1	ı	·	:	1		1
5	Coal		Wall-fired/PC	>250	009	0	;	;	;	:	:		:	;	1	;
25	CoalMood/NFF Liquid/NFF Solid	- •	₹	0.10	. ,	0	٠ .	;	}	1	;	<b>-</b>	,	:	;	ì
8	Coal/Wood/NFF Liquid/NFF Solid		¥	10.100	38	0		:	;	;	1	;	1	:		;
25	COSIMOODINE LIQUIDINE SOLD		₹	100-250	173	0	;	;	;	;	;	1	,	1	;	1
8	Residual Liquid FF	-•	A.	0.10	ო	8	0	0	0	0	0	0	0	С	0	0
8	Residual Liquid FF		A.	10-100	37	23	0	0	0	0	0	0	0	0	0	0
85	Residual Liquid FF		A.	100-250	172	0	0	0	0	0	0		0	0	0	0
83	Residual Liquid FF		Alt	>250	547	0	0	0	O	0	0	0	0	0	0	0
	TOTAL	1年の	The state of the s	19. 经数据保险的	1 34 17 18 1	705	289	14	243	29 √5€	1. 2. 8. 1.	903,221	32,047,732	38,152,062	1,216,197	72,319,212

11/18/02

# Attachment A-12. Comparison of Fuel Switching Costs to Add-on Control Costs

L	かのから はぎのできるからの 一番のからなった。	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	-	The state of the s		Дж. Д	Total Canital	Total Canital Incomesses (6)		, , , , , , , , , , , , , , , , , , , ,
							1	mvesment (4)	lotal Annu	lotal Annual Costs (s/yr)
Model			Capacity Range	Capacity	No. of	No. of	Total Floor	Total Fuel	Total Floor	Total Fuel
2 -	Material	Combustor Type	(MMBtu/hr)	(MMBtu/hr)	Boilers	Heaters	Controls	Switching	Controls	Switching
- ‹	Codi	Other	0-10	4	83	0	0	17,216,016	0	8,216,675
7 (	Coal	Other	10-100	54	616	0	219,124,058	262,258,854	198,377,984	1,003,403,469
. ·	Coal	Other	100-250	166	609	0	232,912,814	336,553,198	156,043,348	1,697,833,339
4	Coal	Other	>250	565	204	0	196,436,023	422,992,860	76,962,031	2,306,934,969
S	Coal	Wall-fired/PC	0-10	2	12	0	0	1,277,558	0	598,902
9	Coal	Wall-fired/PC	10-100	22	98	0	26,917,402	23,237,489	16,467,757	112,456,085
7	Coal	Wall-fired/PC	100-250	186	212	0	108,958,207	146,998,419	67,304,974	791,860,501
ω	Coal	Wall-fired/PC	>250	009	291	0	382,606,184	591,571,540	139,169,534	3,498,591,792
6	Coal/Wood/NFF Liquid/NFF Solid	All	0-10	9	7	0	0	1,604,483	0	978,885
2	Coal/Wood/NFF Liquid/NFF Solid	₽	10-100	35	29	0	31,676,062	22,034,050	6,662,316	48.134.768
=	Coal/Wood/NFF Liquid/NFF Solid	All	100-250	173	18	0	2,301,915	11,716,403	1,598,081	62,572,304
12	Coal/Wood/NFF Liquid/NFF Solid	₽	>250	595	11	0	16,910,191	146,345,808	6,767,664	871,679,071
4	Residual Liquid FF	ΑII	0-10	m	477	75	0	101,309,435	0	23.723.867
4	Residual Liquid FF	All	10-100	37	1,154	516	0	441,699,935	0	705,078,519
42	Residual Liquid FF	- W	100-250	172	264	99	0	190,713,425	Э	547,925,761
43	Residual Liquid FF	All	>250	547	141	17	0	246,011,389	0	726,335,629
47		Other	0-10	4	36	0	7,623,718	9,389,755	1,852,194	1,839,340
48		Other	10-100	54	02	0	30,850,366	15,002,895	7.046,840	26,915,780
<del></del>		Other	100-250	466	59	0	28,960,511	39,839,259	5,252,701	94,862,605
<u>ي</u>		Other	>250	565	7	0	56,000	10,085,356	96,000	27,567,428
52	Coal	Wall-fired/PC	10-100	25	32	0	15,807,877	6,135,600	4,009,020	12,897,842
23		Wall-fired/PC	100-250	186	6	0	7,333,746	7,077,388	1,367,661	11,873,271
\$		Wall-fired/PC	>250	009	15	0	120,000	18,715,031	120,000	62,518,961
£ :		₹	0-10	9	-	0	123,231	276,475	38,165	65,029
20		₹	10-100	35	2	0	585,663	698,486	131,893	534,196
) ç	quid/NFF Solid	A <u>i</u>	100-250	173		0	8,000	748,155	8,000	1,228,670
G ;		- A	0-10	ო	159	80	0	18,676,639	0	5,439,782
5 8		₩	10-100	37	304	23	0	44,821,420	0	96,946,284
87		₹	100-250	172	63	0	0	33,227,462	0	76,183,650
28	Kesiqual Liquid FF	70,000 %	>250	547	7	0	0	6,787,477	0	26,540,852
· ·	TOTAL		このでは、一般の一般の一般の一般の一般の一般の一般の一般の一般の一般の一般の一般の一般の一	ないとなるでは	5,268	705	~705 4 41,309,311,968	₹3,175,022,259₹	- 689,236,164	12,851,738,227

Appendix A-13. Fuel Switching Emission Reductions For Each Boiler Model.

		Model Parame	meters						S	Selected HAPs	Ps				
epow ON	Material	Combustor Type	Capacity Range (MMBtu/hr)	Average Capacity (MMBtu/hr)	No of Bollers	Acetaldehyde	Arsenic anaxoaA	Benzene Chromium	Formaldehyde	Hydrochloric Acid	hydrofluoric Acid	peaq	Manganese	Метсигу	Toluene
-	Coal	Other	0-10	4	83						***				
7	Coal	Other	10-100	54	919	-27 82 1	517 1	27 16	53 -29 89	-	400 99	_	90 34	0 62	1.74
m	Coal	Other	100-250	167	509	47 44 1	26	2 13 20 16				26 08	110 57		2 91
4	Coal	Other	>250	565	204	-64 98 1	5 49 2	80 16	70 -69 62	2 11311 67	7 718 25		92 34	1 43	3 82
လ	Coal	Wall-fired/PC	0-10	2	12										
9	Coal	Wall-fired/PC	10-100	25	86			٥				1 28	5 45		0 19
7	Coat	Wall-fired/PC	100-250	186	212	18	9	98 4	တ္ဆ				24 44	49	1 33
8	Coal	Wall-fired/PC	>250	009	291	-97 93	1285 4	45 13	65 -105 18	8 19074 27	7 1225 14	18 02	76 77	2 17	6 07
6	Coal/Wood/NFF Liquid/NFF Solid	All	0-10	9	7		***								
2	Coal/Wood/NFF Liquid/NFF Solid	¥	10-100	35	29			0		7134	72 01	0 76	4 53	0 0 1	0.00
=	Coal/Wood/NFF Liquid/NFF Solid	₽	100-250	173	18		14	29 42 0 3				0	2 30		000
12	Coal/Wood/NFF Liquid/NFF Solid	Ail	>250	565	77	180 63	1 25   442	442 45 27	71 445 38	8 1211 09	1103 48	_	20 27	0 19	000
40	Residual Liquid FF	All	0-10	က	477										
4	Residual Liquid FF	All	10.100	37	1154			2			000	1 49	130 58	98	3 55
45	Residual Liquid FF	All	100-250	172	264		49	7		ςς.	000	1 49	130 68	91	3 77
43	Residual Liquid FF	Ail	>250	547	141	-45.26	0.88	1.38 50	08 -35 89	9 10.33	000	2 69	235 35	1 55	6 44
47	Coal	Other	01-0	4	36					<b>**</b>					
48	Coal	Other	10-100	54	02	_	25	0	28 -0 38	_	5.51	0 36	1 52		0.02
49	Coal	Other	100-250	167	53	-0 45	_	0	9		707	0 44	187		0 03
22	Coal	Other	>250	565	2						4 95	0.04	0 19		0.02
25	Coal	Wall-fired/PC	10-100	25	32		0 13 0.	0	14 -0 18	32 84	2 39	0 18	0 78		0 01
53	Coal	Wall-fired/PC	100-250	186	6			0.01 0.0	09 -0 17		2 40	0.12	0 20		0.01
54	Coal	Wall-fired/PC	>250	909	15	-	0	04 00	06 0- 20	183.57	12 02	0 10	0.43	0.02	0.05
55	Coal/Wood/NFF Liquid/NFF Solid	ΑII	0.10	9	-								***	886	
99	Coal/Wood/NFF Liquid/NFF Solid	Aii	10-100	35	2	_		8	0	0 30	0.31	000	05		000
23	Coal/Wood/NFF Liquid/NFF Solid	All	100-250	173	-	0 08	0 00 0	20 0 00	0 20	-	0 54	000	0 01	00 0	000
80	Residual Liquid FF	All	0-10	က	159	*			<u> </u>				333	233	
8	Residual Liquid FF	A	10-100	37	304						8	0 0 2	2 80		0 16
85	Residual Liquid FF	All	100-250	172	63	90	0.02 0	0 03 0 12	12 -0 84	0.24	0.00	0 07		0.04	0.15
83	Residual Liquid FF	Aii	062<	547	,	-0.37		ᅰ	ᆀ	-	0.00	0.02	2.03		0.00

Appendix A-14. Fuel Switching Emission Reductions For Each Process Heater Model.

	子会会) Model I	Model Parameters	2							Selec	Selected HAPs	Ps				
Model No	Material	Combustor Type	Capacity Range (MMBtu/hr)	Average Capacity (MMBtu/hr)	No of Heaters	ebyfiebistecA	Arsenic	Benzene	Chromium	Formaldehyde	Hydrochions Acid	Hydrofluoric Acid	peaq	əsəueBuew	Mercury	Toluene
-	Coal	Other	0-10	4	0											
~	Coal	Other	10-100	54	0	0.00	000	000	000	00 0	00 0	000	00 C	0000	00 0	000
ო	Coal	Other	100-250	167	0	0.00	000	00 0	000	0.00	000	000	00 0	000	00 0	00 0
7	Coal	Other	>250	595	0	0.00	000	00 0	000	000	0000	000	000	000	000	000
2	Coal	Wall-fired/PC	0.10	2	0											
9	Coal	Wall-fired/PC	10-100	25	0	00 O	000	0000	000	0000	000	000	00 0	000	000	000
^	Coal	Wall-fired/PC	100-250	186	0	0.00	000	00 0	0000	0.00	000	000	000	000	000	000
8	Coal	Wall-fired/PC	>250	009	0	000	000	000	00.0	000	0000	0000	000	000	000	000
<u>ග</u>	Coal/Wood/NFF Liquid/NFF Solid	All	0-10	9	0											
2	Coal/Wood/NFF Liquid/NFF Solid	A!!	10-100	35	0	000	00 0	00 0	00 0	000	000	000	00 0	000	000	000
=	Coal/Wood/NFF Liquid/NFF Solid	ΑĪ	100-250	173	0	000	000	000	00 0	00.0	00 0	000	0000	000	000	000
12	Coal/Wood/NFF Liquid/NFF Solid	₽	>250	565	0	0.00	000	00 0	00.0	0.00	00 0	000	000	0000	000	000
4	Residual Liquid FF	Ŧ	0-10	3	75				ľ							
4	Residual Liquid FF	¥.	10-100	37	516	-11 20	0 22	0 34	1 30	-8 89	2 54	000	69 0	60 10	0 38	1 59
45	Residual Liquid FF	₹	100-250	172	99	99 9-		0 20	0.78	-5.28	1 52	00 0	0 41	36 07	0 23	0.95
43	Residual Liquid FF	All	>250	547	17	-5.46	0.11	0 17	0 64	4.33	1 25	00 0	0 34	29 55	0 19	0 78
4	Coal	Offher	0-10	4	0											
84 3	Coal	Other	10-100	54	0	000	000	00 0	00 0	00.00	00 0	00 0	00 0	00 0	000	000
4 0	Coal	Other	100-250	167	0	000	000	00 0	000		00 0	000	000	000	000	00 0
2 8	Coal	Omer Wall food/DC	>250	565	0 (	9 8	000		000		0.00	000	000	000	000	000
	Sec C	Wall-lifed/PC	100 250	26,	<b>)</b>	00.0	000		00.0	00 5	000	000	000	9 0 0	000	00.0
25	Coar	Wall-lired/PC	2050	901	<b>&gt;</b> <	200	3 8	3 8	9 8		00 0	0000	000	000	000	00 0
55	Coal/Wood/NFF Liquid/NFF Solid	All	0-10	9		3	200	- 8	3	200	000	000	000	000	000	000
56	Coal/Wood/NFF Liquid/NFF Solid	Ā	10-100	. £	o c	000	0	9			2					
25	Coal/Wood/NFF Liquid/NFF Solid	All	100-250	173	0	000	000		8 0		8 0	3 8	3 8	8 8		3 6
80	Residual Liquid FF	Ail	0-10	3	8			***					3			3
81	Residual Liquid FF	Ŧ	10-100	37	23	-0 08	-	-	<del>3</del> —	-0 07	0 02	000	0.01	3	00.0	0 01
85	Residual Liquid FF	F F	100-250	172	0	000	00 0	00 0	0000		000	000	0000		000	00 0
ဒ	Residual Liquid F.F.	All	>250	547	0	00.0	$\dashv$	ᅱ	$\dashv$	000	-	00 0	00 0		000	00 0

Appendix A-15. Comparison of Emission Reductions From Fuel Switching vs. Add-on MACT Controls

						Metals	s						Acid Gases	1505				And a second sec	Organics	nics			
		Ars	Arsenic	Chromium	nlum	Lead	ם	Manganese	nese	Mercury		Hydrogen Chloride	Chloride	Hydrogen Fluoride	Fluoride	Acetaldehyde	hyde	Benzene		Formaldehyde	ehyde	Toluene	je P
Combustar Fuel	Fuel	Fuel Switch	MACT	Fue! Switch	MACT	Fuel Switch	MACT	Fuel Switch	MACT	Fuel	MACT	Fuel Switch	MACT	Fuel	MACT	Fuel Switch	MACT	Fuel	CT	Fuel	MACT	Fuel	MACT
Boiler	Coal	7.0	Rt*	11	7,	Jŷ1	ŝ	+32	297	6.1	1.5	53,216	37.036	4,583	2.400	70	כ	505	0	211	0	91	0
	Hesidual	2	0	=	0	5.8	Э	510	0	3.4	0	22	0	0	0	100	5	30	0	8.	0	2	0
	Fotal	72	7	ĝ	7.0	100	3	943	297	9.2	1.5	53,238	37 036	4.583	2,400	3		909	0	132	0	99	ာ
Process	Coal	0	0	0	э	0	0	0	0	0	0	0	0	0	0	э	Э	0	0	0	0	o	0
Heaters	Hesidual	0.5	0	2.7	2	7 -	0	126	٥	80	0	5.3	0	c	0	6.7	2	0.7	0	61.	0	33	0
	Fotal	0.5	0	17	Э	7	.p	126	0	9.0	0	53	0	0	0	ξ,	Q.	20	0	61.	0	e 5	0
Fotal	Coal	0/	87	"	7.	3	S	432	297	6.1	9 1	53,216	37,036	4.583	7.40v	3	2	506	0	211	o	5	0
_	Hesidual	2.5	٥	7	)	12	0	636	0	4.2	0	27	0	0	9	123	, j	3.7	0	86.	0	17	0
	Fotal	73	97	5	3	10/	ĘĢ	1,069	297	2	5	53,243	37,036	4.583	7. 100,	18/	0	609	0	113	0	33	0